

Table I
Results of Polymerization of Indene and Styrene

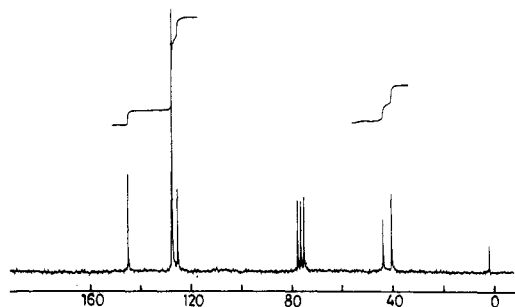
polymer	polym time, h	polym yield, mg	styrene content, mol %	T_g , °C
polystyrene ^a	3	180		96
polyindene ^b	46	30		160
poly(styrene-indene) ^c	47	77	52.9	126

^a Polymerization conditions: polym temp = 60 °C; styrene = 10 cm³; Ti(OⁱPr)₄ = 0.1 mmol; MAO = 2.0 mmol; toluene = 29 cm³.

^b Polymerization conditions: polym temp = 60 °C; indene = 37 cm³; Ti(OⁱPr)₄ = 0.1 mmol; MAO = 2.0 mmol. ^c Polymerization conditions: polym temp = 60 °C; styrene = 3.3 cm³; indene = 33 cm³; Ti(OⁱPr)₄ = 0.1 mmol; MAO = 2.0 mmol.

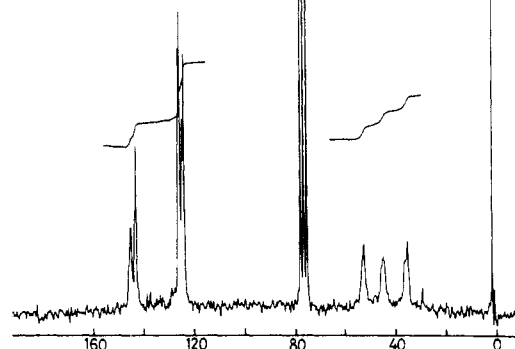
(a)

Polystyrene



(b)

Polyindene



(c)

Poly(styrene-indene)

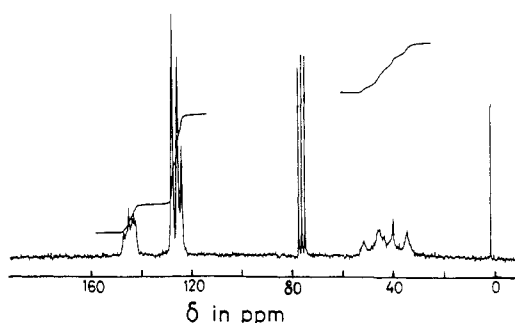


Figure 1. ¹³C NMR spectra of the polymers. (a) Polystyrene: polym temp = 60 °C; styrene = 10 cm³; Ti(OⁱPr)₄ = 0.1 mmol; MAO = 2.0 mmol; toluene = 29 cm³. (b) Polyindene: polym temp = 60 °C; indene = 37 cm³; Ti(OⁱPr)₄ = 0.1 mmol; MAO = 2.0 mmol. (c) Poly(styrene-indene): styrene content = 52.9 mol %; polym temp = 60 °C; styrene = 3.3 cm³; indene = 33 cm³; Ti(OⁱPr)₄ = 0.1 mmol; MAO = 2.0 mmol.

content of styrene unit in the copolymer was calculated from the spectrum (c).

Both T_g and molecular mass distribution (MMD) were measured on the copolymer. The results obtained are shown in Table I and Figure 2. The copolymer displays a new T_g (126 °C) between those of polystyrene (96 °C) and polyindene (160 °C), and its MMD is unimodal with a very narrow polydispersity. Thus the polymer obtained

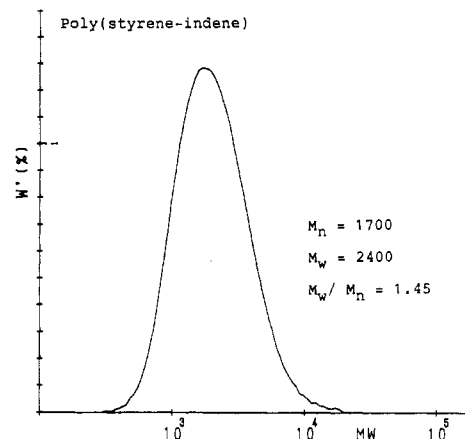


Figure 2. MMD curve of the copolymer (c).

from the copolymerization can be regarded as a random copolymer of styrene and indene.

When polymerization of styrene is carried out with usual cationic catalysts, atactic polystyrene is obtained by a cationic mechanism. Judging from both the present and previous⁶ results, we propose a coordinated-cationic mechanism for syndiotactic polymerization of styrene.

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Kazuo Soga*

Research Laboratory of Resources Utilization
Tokyo Institute of Technology, 4259 Nagatsuta
Midori-ku, Yokohama 227, Japan

Takashi Monoi

Oita Research Laboratory, Showa Denko K.K., 2
Nakanosu, Oita 870-01, Japan

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Perfect Conversion of Aspecific Sites into Isospecific Sites in Ziegler-Natta Catalysts

Introduction. The catalyst system composed of Solvay-type TiCl₃ and Cp₂TiMe₂ was found to show extremely high isospecificity for olefin polymerization.¹ The isospecificity of donor-free TiCl₄/MgCl₂ catalysts was also improved to a great extent by using Cp₂TiMe₂ as co-catalyst.²

Usual MgCl₂-supported TiCl₄ catalysts combined with AlEt₃ do not show high isospecificity, but they give at least

Table I
Results of Propylene Polymerization over MgCl₂-Supported Catalysts Combined with AlEt₃ as Cocatalyst

catalyst	TEA, mmol/dm ³	temp, °C	time, h	activity, ^a kg of PP/g of Ti per h	II, ^b %
Cat-A ^c	20	40	1	127.0	0
Cat-B ^d	10	40	1	96.2	26

Pentad Distributions (by ¹³ C NMR for Total Polymers)									
	mmmm	mmmr	rmmr	mmrr	mrrm	rrmr	rmrm	rrrr	mrrr
Cat-A	34.7	12.9	2.2	14.1	10.3	2.6	8.9	6.8	7.5
Cat-B	57.2	8.1	0.9	9.0	5.8	1.8	7.7	4.9	4.6
K-Cat ^e	6	13	6	13	25	13	6	13	6

^a Average activity for the initial 1 h. ^b Isotactic index determined by fractionation with boiling heptane. ^c TiCl₃/MgCl₂ catalyst (Ti content = 0.043 wt %) prepared by treating the mixture of MgCl₂ and TiCl₃·3Py with Al₂Et₃Cl₃. ^d TiCl₄/MgCl₂ catalyst (Ti content = 0.40 wt %) prepared by treating MgCl₂ with TiCl₄. ^e Polypropylene obtained with a typical Kaminsky catalyst (Cp₂TiPh₂/methylaluminoxane, at 50 °C).⁸

20 wt % of isotactic polypropylene even in the absence of any Lewis bases. Production of isotactic polymer might result from the multinuclear Ti³⁺ species formed on the MgCl₂ surface.^{3,4}

A marked decrease in the Ti content may avoid the formation of such an isospecific multinuclear Ti³⁺ species and selectively give an aspecific mononuclear Ti³⁺ species on the MgCl₂ surface. In fact, we found that the isospecificity of MgCl₂-supported catalysts decreases with a decrease in the Ti content.⁵

More recently, we have succeeded in preparing a completely aspecific catalyst from TiCl₃·3Py (Py = pyridine) and MgCl₂ in the presence of Al₂Et₃Cl₃. By changing the cocatalyst from AlEt₃ to Cp₂TiMe₂, the catalyst was easily converted into a highly isospecific catalyst. This communication reports the brief results of propylene polymerization with this catalyst system.

Experimental Section. Materials. Propylene (from the Mitsubishi Petrochemical Co.), MgCl₂, and titanium-reduced TiCl₃ (from the Toho Titanium Co.) were used without further purification. Research-grade heptane commercially obtained was purified according to the usual procedures. Cp₂TiMe₂ was prepared according to the literature reported by Clauss et al.,⁶ diluted into 0.25 mol/dm³ in heptane, and stored as stock solution.

Preparation of the MgCl₂-Supported Catalysts.
Cat-A. TiCl₃·3Py was prepared from the reaction of TiCl₃ with pyridine at room temperature. A total of 30 g of MgCl₂ (11 m²/g) was ground in a 1-dm³ stainless steel vibration mill pot with 50 balls (25 mm in diameter) under nitrogen for 48 h at room temperature. The mixture of the resultant MgCl₂ (10 g, 97 m²/g) and TiCl₃·3Py (36 mg) was treated with an excess amount of Al₂Et₃Cl₃ (10 mmol) in heptane at 0 °C under vigorous stirring, followed by washing with plenty of heptane to obtain the TiCl₃/MgCl₂ catalyst. It was confirmed from the elemental analysis that pyridine was completely removed from the catalyst.

Cat-B. A total of 5 g of the same MgCl₂ (97 m²/g) was brought into contact with a diluted solution of TiCl₄ in heptane at room temperature for 2 h. The solid part was isolated by filtration and washed several times with heptane at room temperature to obtain the TiCl₄/MgCl₂ catalyst.

Polymerization and Analytical Procedures. Polymerization of propylene was usually conducted at 40 °C in a 0.1-dm³ stainless steel autoclave reactor equipped with a magnetic stirrer. Measured amounts of the catalyst and cocatalyst (AlEt₃ or Cp₂TiMe₂) were added to the reactor containing 0.05 dm³ of heptane. Propylene (0.3 mol) was introduced to the reactor at liquid-nitrogen temperature. Polymerization was terminated by adding a dilute hydrochloric acid solution in methanol. The polymer was

fractionated by extraction with boiling heptane. The contents of titanium in the catalysts were determined by atomic absorption spectrophotometry (Shimadzu AA-6105). The ¹³C NMR spectrum of the polymer was recorded at 120 °C using a JEOL GX-270 spectrometer in the pulse Fourier transform (FT) mode. Sample solutions were made in 1,2,4-trichlorobenzene/benzene-*d*₆ (9/1 by volume) up to 12% by weight.

Results and Discussion. As mentioned above, usual MgCl₂-supported catalysts combined with AlEt₃ give more than 20 wt % of isotactic polypropylene. Whereas, the catalyst containing 0.12 wt % of Ti, which was prepared with the same procedures as Cat-A, was found to afford only 6 wt % of isotactic polypropylene.⁴ From such a viewpoint, the content of Ti was decreased to 0.043 wt % in the present study. Polymerization of propylene was carried out at 40 °C by using the catalyst (Cat-A) and AlEt₃. The polymer produced was fractionated by extraction with boiling heptane for 10 h to obtain no insoluble fraction. The DSC curve of the polymer did not show a sharp peak at around 160 °C attributable to crystalline isotactic polypropylene but displayed a very broad peak centered at 140 °C.

Polymerization of propylene was also conducted by using Cat-B and AlEt₃ under the same conditions, which gave an appreciable amount of isotactic polypropylene. In Table I are shown the polymerization results and the pentad sequence distributions of the polymer. The pentad sequence distributions of polypropylene obtained with a typical Kaminsky catalyst is also shown as reference. It is clear from Table I that the structure of the present atactic polypropylene (obtained with Cat-A) is significantly different from that obtained with a homogeneous Kaminsky catalyst.^{7,8} The former contains both isotactic and syndiotactic sequences, while the latter has a perfectly random, statistically atactic structure. However, the present polymer might also be called "atactic polypropylene".

The difference in the isospecificity between the Cat-A and Cat-B may be interpreted as follows. In case of the Cat-A, by treating the mixture of MgCl₂ and TiCl₃·3Py with a Lewis acid like Al₂Et₃Cl₃, the pyridine coordinated with TiCl₃ is removed, resulting in formation of the isolated mononuclear TiCl₃ species on the MgCl₂ surface. Even in case of the Cat-B, most of the TiCl₄ supported on the MgCl₂ surface might be originally mononuclear species, taking the Ti content into consideration. However, reduction of the Ti⁴⁺ species to Ti³⁺ is necessary to activate the catalyst.⁹ When strong reducing reagents like AlEt₃ are used as cocatalyst, the reduction may proceed instantaneously, resulting in formation of an appreciable amount of labile alkyltitanium species on the MgCl₂ surface. Such

Table II
Steric Pentad Sequence Distributions of Polypropylene Obtained from $\text{TiCl}_3/\text{MgCl}_2$ (Cat-A) Combined with Cp_2TiMe_2 as Cocatalyst^a

polymer fractions	mmmm	mmmr	rmmr	mmrr	mmrm rrmr	rmrm	rrrr	mrtrr	mrrm
whole polymer	89.4	3.0	0.6	1.8	1.2	0.3	2.1	0.7	0.9
I-7 (95%) ^b	94.5	1.6	0.3	0.7	0.6	0.2	1.2	0.4	0.5

^a For the polymer obtained with $20 \text{ mmol} \cdot \text{dm}^{-3}$ of Cp_2TiMe_2 at 40°C . ^b I-7 denotes boiling heptane insoluble part.

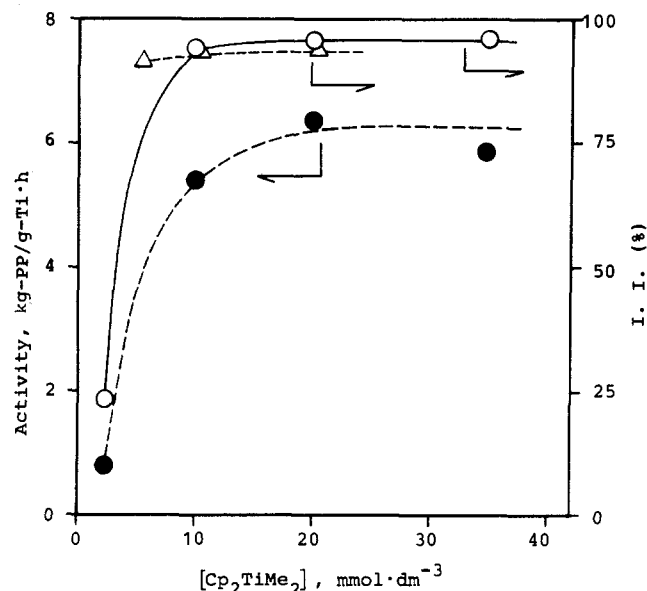


Figure 1. Effects of $[\text{Cp}_2\text{TiMe}_2]$ on the yield (●) and isotactic index (○) of polypropylene obtained with the $\text{TiCl}_3/\text{MgCl}_2$ (Cat-A)- Cp_2TiMe_2 system. The isotactic index of polypropylene obtained with the $\text{TiCl}_4/\text{MgCl}_2$ (Cat-B)- Cp_2TiMe_2 system is shown for reference (Δ).

labile titanium species might easily aggregate with each other to form the multinuclear species, which give isotactic polypropylene.

Although we must investigate the surface structures of these catalysts in detail to check the validity of the above assumption, we could prepare a completely aspecific MgCl_2 -supported catalyst (Cat-A).

Then, polymerization of propylene was conducted under similar conditions by using Cp_2TiMe_2 as cocatalyst. Polymerization results are illustrated in Figure 1. With an increase in the concentration of Cp_2TiMe_2 , catalyst isospecificity markedly increased to reach as high as >95%. Polymerization with Cat-A at a very low concentration of

Cp_2TiMe_2 might proceed over different active species that were formed in the process of the treatment with $\text{Al}_2\text{Et}_3\text{Cl}_3$.⁵ The pentad sequence distributions of the polymers obtained by Cat-A and Cp_2TiMe_2 are shown in Table II, indicating that the catalyst isospecificity is very high. Typical results obtained with Cat-B and Cp_2TiMe_2 are also shown in Figure 1 for reference. Thus, the isospecificity of a donor-free MgCl_2 -supported catalyst (Cat-A) is easily converted from aspecific into isospecific by changing the cocatalyst. However, the activity decreased drastically by changing the cocatalyst from AlEt_3 to Cp_2TiMe_2 . Supposing that the propagation rate of isotactic polymerization is faster by 1 order of magnitude as compared with that of atactic polymerization,¹⁰ it may be said that most of the potentially active sites are not still activated by Cp_2TiMe_2 . From such a viewpoint, we are now investigating how to activate the present catalyst. If it will be successful, the present catalyst system may be most suitable for the precise characterization of both aspecific and isospecific sites in Ziegler-Natta catalysts.

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Kazuo Soga,* Joon Ryeo Park, Hideshi Uchino,
 Toshiya Uozumi, and Takeshi Shiono

Research Laboratory of Resources Utilization
 Tokyo Institute of Technology, 4259 Nagatsuta
 Midori-ku, Yokohama 227, Japan

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